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⑤④ **Process for removing water soluble organic compounds from produced water.**

⑤⑦ A process for the removal of water soluble organic compounds from produced water is provided. The process allows for the removal of water soluble organic compounds by passing the produced water through a column of adsorbing resin which is capable of removing the soluble organic compounds from the water and providing an environmentally acceptable effluent. The removal of pollutants from the produced water is monitored continuously by a fluorescence detector. The process further allows for the regeneration of the adsorbing resin by regenerating the resin with a solvent capable of eluting accumulated soluble organic compounds from the column followed by treatment of the resin with steam to remove residual eluting solvent. The process further allows for the treatment of the eluting solvent and soluble organic compound admixture in a manner to allow reuse of the solvent and to allow recovery of the soluble organic compounds or to allow direct injection of the soluble organic compound admixture into the oil stream. Thus, the invention provides a process for removal and recovery of water soluble organic compounds from produced water which creates no environmentally hazardous waste streams.

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BACKGROUND OF THE INVENTION

The following disclosure is a continuation-in-part of previously filed U.S. Patent Application Serial No. 451,219, filed December 15, 1989.

The present invention relates to a process for the removal of water soluble organic compounds from water. The invention further relates to a process for the removal of water soluble organic compounds associated with the production of crude oil. The invention further relates to a means of recovery of the soluble organic compounds present in produced water.

In the process of crude oil production from subterranean formations, a substantial amount of water may be produced. Such oil-associated water (produced water) contains contaminating compounds which must be removed prior to releasing the water into the environment. Of course, it is possible to use turbidometric or colorimetric procedures to test for the content of oil in such water. However, in many instances, the contamination in the water is not visible to the naked eye since many of the pollutants are water soluble and, therefore, require detection methods capable of monitoring these compounds. For example, Environmental Protection Agency regulations currently stipulate a maximum oil content of 48 parts per million (ppm) for produced water released into surface waters of the Gulf of Mexico and Pacific Ocean (Fed. Reg. 51, 24897, July 6, 1986).

Other sources of produced water are encountered in the refining of crude oil. Plants which process oil products are increasingly limited by federal and state regulations as to the total organic content (soluble and dispersed hydrocarbons) of effluent water. Additionally, certain production facilities such as steam-generation plants, typically require large amounts of deionized water for processing. Since shortages of freshwater routinely occur in semiarid and desert regions, facilities located in these areas must provide their own source of water.

Older techniques for dealing with contaminated water involved reinjection into wells or percolation through a series of treatment ponds. These methods were unacceptable due to their high costs and environmental damage. Even so, these techniques continue to be used where no economical options exist.

More modern methods of removing oil and water soluble organics from produced water have been previously described. Canadian Patent 1,103,170 relates to the use of a macroporous, cross-linked polymer adsorbent in columns capable of preferentially adsorbing oil. The patent further relates to the addition of pH adjusting agents coupled with a non-ionic surfactant to remove the adsorbed oil from the column. Additionally, the patent relates to the further alteration of the pH and to the final separation of the oil from the surfactant by phase separation techniques. The method taught by this patent, apart from including several intermediate steps in the purification and recovery process, has the disadvantage of requiring acidification during the processing thereby generating additional pollutants.

Two recent U.S. Patents (4,818,410 and 4,839,054) relate to methods for removal of water soluble organics from produced water by acidification, mixing, and phase separation. Similarly to Canadian Patent 1,103,170, these methods include several intermediate steps in the purification and recovery process. Moreover, these patents relate to the use of strong acids, thereby adding pollutants to the process stream.

U.S. Patent 4,775,475 relates to the removal of trace amounts of hydrocarbonaceous compounds from aqueous feedstreams by contacting the feedstream with a suitable adsorbent such as molecular sieves, amorphous silica-alumina gel, silica gel, activated carbon, activated alumina and clays. This patent relates further to the regeneration of these adsorbents by contacting with an elution solvent such as naphtha, kerosene, diesel fuel, gas oil or mixtures of these solvents. In further steps, this patent relates to the treatment of the hydrocarbonaceous compound and elution solvent admixture in the presence of hydrogen with a hydrogenation catalyst, further treatment with an aqueous scrubbing solution which preferably contains a strong base, and still further treatment by phase separation. The resulting spent aqueous scrubbing solution requires neutralization or other treatment prior to releasing into the environment.

One typical method utilized to overcome some of the adverse characteristics of the systems which generate additional pollutants is based upon activated carbon filtration. In an activated carbon system, the carbon must be routinely removed from the filter. After removal, the carbon is either regenerated outside the filter by heating to high temperatures or it is simply discarded and replaced with new material. Additional problems with activated carbon filters arise due to microbial growth on the carbon matrix itself.

More recently, a variety of improved matrices have been designed which overcome some of the limitations encountered with activated carbon, such as the macroporous resins. Generalized procedures relating to the use of macroporous resins are also known which are directed to the removal of organics from fluids. See, e.g., U.S. Patent 4,297,220.

In all such systems, a variety of means are taken to monitor the treated produced water in order to

ascertain: (1) the efficacy of the treatment procedures; and, (2) the compliance of the treatment with federal and state regulations. Typically, these methods are carried out by spot-checking the effluent treated water by a variety of standard methods for examination of water such as Standard Method 5520 B (503 A - Partition-Gravimetric Method) or Standard Method 5520 C (503 B - Partition-Infrared Method). see e.g.,
 5 "Standard Methods for Examination of Water and Waste Water" Port City Press, Baltimore Md, pp. 5-43 to 5-44 (1989).

Again, such methods suffer from a number of disadvantages when used in treatment systems for removal of pollutants from produced water. Chlorinated hydrocarbon solvents as well as strong acids must be added to the water in order to extract the solubilized oil constituents. Furthermore, there is no convenient
 10 way in which these methods can be utilized in a continuous monitoring system in order to obviate the necessity of spot-checking filters for the breakthrough level at which point regeneration must be achieved.

Effluent monitoring of oil in water has been accomplished for industrial plant effluents using turbidimeters and fluorescence meters, see, e.g. K. Coursin, "Effluent Monitoring for Oil in Water." Pollution Engineering 20:100-102 (1988). However, integrated systems are needed which allow environmentally safe
 15 and real-time monitoring of soluble organic concentrations in produced water regardless of salt concentrations in the water. Preferably, such systems will combine a total oil removal process with a system capable of automation which allows continuous monitoring of the efficiency of the purification.

Such improved systems should accurately monitor breakthrough of threshold levels of pollutants which indicate necessity of regeneration of the treatment means regardless of whether this breakthrough occurs
 20 as a result of discontinuous oil concentrations in the water to be treated or whether it occurs due to a treatment system failure. Such systems should not be based on time or on volume of effluent but rather they should be based on effluent oil concentration. In addition, such systems should best be automatable such that no human error or down time due to analysis is evident. These requirements are of particular concern where, such as in offshore production operations, alternative methods can dramatically increase
 25 costs, waste man-hours and enhance the probability for accidental contamination of the marine environment due to human error.

The present invention therefore provides a process for removal of water soluble organic compounds from produced water as defined herein, which is characterized by the steps of directing a stream of produced water into a first column of adsorbing resin capable of accumulating water soluble organic
 30 compounds from the produced water and capable of producing an effluent with a reduced concentration of water soluble organic compounds; monitoring the concentration of water soluble organic compounds in the effluent of the first column of adsorbing resin; redirecting the stream of produced water into an alternate column of adsorbing resin capable of removing the water soluble organic compounds from the produced water and capable of producing an effluent having a reduced concentration of water soluble organic
 35 compounds; monitoring the concentration of water soluble organic compounds in the effluent of the alternate column of adsorbing resin; contacting the first column of adsorbing resin, which has accumulated water soluble organic compounds from the produced water, with a solvent capable of eluting accumulated amounts of the water soluble organic compounds from the adsorbing resin and capable of regenerating the adsorbing resin; redirecting the stream of produced water into the first column of adsorbing resin which has
 40 been regenerated as stated above; and, contacting the alternate column of adsorbing resin, which has accumulated water soluble organic compounds from the produced water, with a solvent capable of eluting the accumulated amounts of water soluble organic compounds from the adsorbing resin and capable of regenerating the adsorbing resin.

One of the advantages of the present invention is that it provides a process for the removal of water
 45 soluble organic compounds from produced water which does not require the additional steps of mixing and phase separation nor the introduction into the process stream of pH adjusting agents. Furthermore, the present invention also provides a method which allows the *in situ* regeneration of the filter matrix without the need for removal or high temperature treatment. Additionally, due to the antimicrobial nature of the regenerating solvents, microbial growth on the matrix is prevented.

In a preferred embodiment wherein purification process of the invention is combined with a continuous
 50 fluorescence detection device, the process of the invention further allows a real-time monitoring or pollutant accumulation which is not based on arbitrary timing- or volume-based analytical methods. In so doing, the invention overcomes a substantial problem encountered with prior art methods which either risked missing breakthrough points allowing pollutant-carrying water into the environment or required intensive man-hours
 55 to adequately monitor, analyze and exchange spent filtration systems.

A further aspect of the invention relates to regeneration of the adsorbing resin by contacting with a solvent capable of eluting accumulated soluble organic compounds from the column followed by treatment of the resin with steam to remove residual solvent. The invention further relates to the treatment of the

eluting solvent and soluble organic compound admixture in a manner to allow reuse of the solvent or direct injection of the spent solvent into the oil stream and to allow recovery of the soluble organic compounds. Thus, the invention provides a process for removal and recovery of water soluble organic compounds from produced water which generates no environmentally hazardous waste streams.

5 Further features and advantages of the invention will become more apparent from the following description of preferred embodiments of the invention taken together with the accompanying drawings wherein:

Figure 1 is a schematic flow diagram depicting the sequence of steps provided by the process of the present invention; and

10 Figure 2 is a comparison of standard methodology for determination of oil in water (soluble organics) versus fluorescence monitoring for produced water from a California production facility using the filter system of the invention in combination with the continuous fluorescence monitor.

The present invention provides a process for removal of water soluble organic compounds from produced water. In general, the water soluble organics are those compounds dissolved as metal salts of oxygenated hydrocarbons, alkane acids, cyclic acids and long chain organic acids. In particular, the water soluble organics include naphthenates, carboxylates, phenols, and aromatic acids typically encountered in produced water. Because of their role as a chief pollutant in produced water, naphthenic acid or any of its salts, of the general formula $R(CH_2)_nCOOH$ where R is a cyclic nucleus of one or more rings or a straight hydrocarbon chain, are of particular concern.

20 Produced water as used here refers to any water produced by industrial processes which generate aqueous waste streams containing contaminating trace amounts of oil and water soluble organic compounds associated with oil. A principal source of such waste water is that water produced from an oil well as a byproduct of crude oil production. Another source of such waste water is that water generated as a result of an oil refining process.

25 In addition to the presence of water soluble organic compounds, produced water which is treatable by the process of the invention may contain dissolved hydrogen sulfide and carbonate compounds. Such additional contaminants are typically encountered in produced water from oil wells. The produced water treated by the process of the invention may also be water which has been pre-treated by deionization, softening, filtration, de-gasification, or by blending with an alternate water source. Produced water pre-treated by a water softening process has been found to provide enhanced results using the process of the invention.

30 The process of the invention further relates to the use of adsorbing resins contained within columns through which the produced water stream is directed. The adsorbing resins of the invention are those resins capable of accumulating water soluble organic compounds from the produced water stream and capable of producing an effluent with a reduced concentration of the soluble organic compounds. Adsorbing resins of particular utility for the purposes of the invention are those which are nonionogenic, macroreticular adsorption resins.

35 In a preferred embodiment, a macroreticular, nonionogenic resin will be used which is constructed of the polymer polystyrene cross-linked with divinylbenzene. The most preferred such resin is the XAD-16 resin of the Rohm and Haas Company (Rohm and Haas Co., Independence Mall West, Philadelphia, PA 19105). Methods for making and using such resins are detailed in U.S. Patent 4,297,220 and related patents.

40 The process of the invention provides for removal of water soluble organic compounds in a relatively few steps without the need for mixing, phase separation or chemical treatment with strong acids and bases. Initially the stream of produced water is directed into a first column which contains a bed of the adsorbing resin chosen for its ability to bind the water soluble organic compounds of interest. Having passed through the adsorbing resin bed in the first column, the resulting effluent from the first column has a substantially reduced concentration of the soluble organic compounds. The effluent may then be fed into an effluent stream for immediate release into surface water or stored for use in subsequent processes requiring purified water.

50 A monitoring step immediately downstream of the first column allows the determination of the water soluble organic compound concentration. This step serves a dual purpose in that it allows control and verification of the water quality for regulatory purposes. The monitoring step also serves as a method for determining when the adsorbing capacity of the adsorbing resin has been reached.

55 The monitoring steps of the invention whereby the concentration of water soluble organic compounds are measured can be any one of several measurements. Such measurement techniques would include but not be limited to measurement of the effluent conductivity, fluorescence, ultraviolet/visible absorption, infrared absorption, and turbidity.

In a highly preferred embodiment, the monitoring steps will be carried out using a fluorescence detector in combination with the process of the invention for removal of water soluble organic compounds. Most importantly, the fluorescence monitoring step should be capable of reproducing consistent readings which compare favorably to spot-checking methods such as those used in Standard Methods 5520 B and C.

5 When the adsorbing capacity of the resin in the first column has been reached, the stream of produced water is redirected so that it enters an alternate column containing the adsorbing resin. It can be appreciated from the nature of the process, that the alternate column may be only one of two such columns or it may be one of a multiplicity of such columns greater than two. The produced water stream entering the alternate column is treated as was that in the first column including a monitoring of the effluent immediately
10 following the alternate column. In this manner, a threshold level can be determined at which the stream of produced water may be redirected into another column containing adsorbing resin with full adsorbing capacity. Thus, in a preferred embodiment, the process of the invention may be carried out in a continuous fashion. In a most preferred embodiment, the entire process of the invention is carried out continuously and automatically.

15 The process of the invention further provides for a regeneration step in which a column which has reached the adsorbing capacity of the resin contained therein is contacted with a solvent capable of eluting the accumulated amounts of the soluble organic compounds from the adsorbing resin, thereby regenerating the adsorbing capacity of the resin. In this manner, the column of resin is readied for subsequent reuse in purifying the stream of produced water. In a preferred embodiment of the invention, the solvent wash is
20 accomplished by backwashing (regenerating) through the column of adsorbing resin in a direction opposite to the direction in which the produced water stream enters the column. In a highly preferred embodiment, the residual solvent left on the column of adsorbing resin will be removed by treating the resin with steam, see, e.g., El-Rifai, et al., Chem Eng 269:26-28 (1973).

The solvent used to regenerate the adsorbing capacity of the adsorbing resins and to recover the water
25 soluble organic compounds from the adsorbing resin may be any one or a mixture of common organic solvents. These solvents may include but are not limited to acetone, isopropanol, ethanol and methanol. Additionally, the solvent may contain an agent capable of removing dispersed oil from the resin such as a non-toxic, non-polluting surfactant. Most preferably when the invention is practiced at remote drilling sites such as drilling sites offshore, the solvent would be a solvent such as methanol which is readily available at
30 such sites due to its routine use in other processes.

In certain applications, a continuous supply of solvent may be available such that there will be no need for solvent regeneration. However, in a preferred embodiment of the invention, the process is self-contained and of limited solvent capacity. Therefore, solvent regeneration is required.

In one embodiment, an additional monitoring step is carried out on the eluting solvent in a reservoir of
35 such solvent in order to determine the concentration of soluble organic compounds therein. At a predetermined level, the spent solvent is exchanged with a fresh solvent. The fresh solvent may be virgin solvent or it may be solvent derived from previous cycles in the process of the invention and which has been regenerated by removing soluble organics. Such monitoring step is achieved by use of a fluorescence detector in a highly preferred embodiment of the present invention. The fluorescence monitoring, in a most
40 preferred embodiment, is continuous.

Regeneration of the solvent may be achieved by any of several methods known in the art. Such methods include but are not limited to distillation, ion exchange, and membrane filtration. In any case, regeneration of the solvent produces a recoverable quantity of the soluble organic removed from the
45 produced water. This recovered product may be stored for use as a raw material source of these compounds or it may be delivered back into the crude oil stream thereby enhancing crude oil production.

In a preferred embodiment, the regeneration of the solvent and the recovery of the organic compounds from the solvent are carried out in a batch or continuous fashion. One such solvent regeneration process involves directing the eluting solvent in a stream through a vacuum distillation apparatus. Such a distillation
50 apparatus is constructed in a manner as to allow the produced water (typically encountered at temperatures greater than 100° F) to be used as a heat source for vaporizing the used solvent. Additionally, an ambient temperature water source such as seawater is used in the apparatus as a heat sink for condensing the purified solvent vapors. The condensed, purified solvent is then returned in a continuous fashion to the central process for use in eluting additional soluble organic compounds from the produced water stream. The soluble organic compounds removed from the solvent may be returned to the crude oil stream or
55 recovered as a source of petroleum carboxylate salts.

Illustrated in Figure 1 is a schematic flow diagram depicting the sequence of steps provided by the process of the present invention. Produced water is introduced 1 and directed 2 into one 3 or another 4 column containing an adsorbing resin. The effluent leaving the resin columns is monitored 5 and the

purified effluent is released from the system 6. At the appropriate time, solvent from a reservoir 7 is pumped 8 and directed 9 through a column in order to regenerate the adsorbing capability of that column. Upon leaving the column, the solvent is monitored 10 and directed into a purifying and recovery system 11 from which the soluble organic compounds are recovered 12 and returned to the crude oil stream and from
 5 which the purified solvent is returned to the solvent reservoir 7.

The following examples illustrate certain aspects of the present invention, including certain preferred embodiments and should not be construed as limiting the claims of the invention. Other embodiments within the scope of the claims of the present invention will be apparent to one of ordinary skill in the art from consideration of the specification or from practice of the invention disclosed herein.

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EXAMPLE 1

A fresh sample of produced water was obtained from an offshore platform in California. This sample was at production temperature (130° F) and was found to contain 300 ppm soluble organics. This
 15 contaminated water was pumped at a flowrate of 2.7 gal/min./ft² through a filter containing 500 g of macroreticular, nonionogenic resin. The filter measured three inches in diameter by 12 inches in height. The results are shown in Table 1 where the soluble organic content (ppm) of the purified water is measured after various volumes of contaminated produced water is passed through the column.

20

TABLE 1

	<u>Total Volume of Water (gal)</u>	<u>Soluble Organic Content (ppm)</u>
25	2.6	67.7
	4.0	73.0
	8.0	92.6
30	13.2	120.7

The filter was drained, backwashed (regenerated) with one gallon of isopropanol, then two gallons of tap water. Another test was performed following the above procedure, using the same produced water, except
 35 at a rate of 5.4 gal/min./ft². The results are shown in Table 2.

TABLE 2

40

	<u>Total Volume of Water (gal)</u>	<u>Soluble Organic Content (ppm)</u>
	2.6	71.4
45	4.0	82.0
	8.0	108.5
	13.2	148.3

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EXAMPLE 2

Another produced water sample was obtained from an oil field in California. This sample was
 55 determined to contain 94 ppm of soluble organics. The filter in Example 1 was used in this test. The flowrate was 2.7 gal/min./ft² at the beginning and increased to 5.4 gal/min./ft² after 10.0 gallons had passed through the filter. Results are shown in Table 3.

TABLE 3

	<u>Total Volume of Water (gal)</u>	<u>Soluble Organic Content (ppm)</u>
5	4.0	18.3
	8.0	21.5
	13.2	38.5

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EXAMPLE 3

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Regeneration lifetime of a resin was tested in the following manner: A 50 g column of resin was prepared. The column was one inch in diameter by 12 inches tall. Two liters of a produced water sample from an offshore platform in California containing 180 ppm soluble organics was run through the column at a flowrate of 9.7 gal/min./ft². A sample of the purified water after 2000 mL total volume was found to contain 35 ppm soluble organics. The column was backwashed (regenerated) at 3-5 gal/min./ft² with 300 mL of isopropanol, followed by 2000 mL of tap water. This procedure was repeated 40 more times. The soluble organics content of the purified water after 2000 mL total volume from the last cycle was found to be 33 ppm.

25 EXAMPLE 4

The effect of column length was compared by running identical tests using a 3-foot and a 5-foot column, both one inch in diameter. This test used the same produced water sample as for Example 3. Both columns were run at a flowrate of 24 gal/min./ft². Results are shown in Table 4.

30

TABLE 4

	<u>Total Volume of Water (mL)</u>	<u>Soluble Organic Content (ppm)</u>	
35		<u>3 ft.</u>	<u>5 ft.</u>
	1000	47.0	21.0
	2000	50.7	30.0
40	3000	59.2	35.3
	4000	62.3	40.1
	5000	66.1	53.9

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EXAMPLE 5

Two liters of a produced water sample obtained from an offshore platform in California containing 87.3 ppm soluble organics was run through the same filter used in Example 3 at a flowrate of 9.7 gal/min./ft². Methanol (300 mL) was used to regenerate the filter in the procedure stated in Example 1. The methanol which contains the soluble organic material was allowed to evaporate at ambient temperature. The soluble organic residue was dissolved in deionized water (100 mL) and acidified to pH 1 with concentrated hydrochloric acid. This acidified sample was extracted twice with 50 mL of freon (trichlorotrifluoroethane). The freon extracts were combined and allowed to evaporate at ambient temperature. The resulting residue weighed 140 mg. Since this residue was extracted from 2000 mL of produced water, this corresponded to 70 mg/liter of soluble organics removed. This represents 80% removal/recovery of the soluble organics as naphthenic acids, since the original produced water sample contained 87.3 mg/liter soluble organics.

EXAMPLE 6

Optimization of the regeneration agent was carried out with the following solvents: acetone, methanol, isopropanol, and 5% aqueous sodium hydroxide solution. Acetone was found to be the best solvent, followed by methanol or isopropanol. Aqueous sodium hydroxide solution (5%) failed to function as an adequate regeneration solvent.

EXAMPLE 7

A produced water sample from a refinery in Alaska was found to contain 307 ppm total organic carbon. A 50 g resin column measuring one inch in diameter by 12 inches in height was used. The flowrate for this test was 9.7 gal/min./ft². Results are shown in Table 5.

TABLE 5

<u>Total Volume of Water (mL)</u>	<u>Total Organic Carbon (ppm)</u>
200	204
400	204
600	202
800	202
1000	228
2000	262
3000	274

EXAMPLE 8

A sample of produced water from a chemical plant in southeast Texas was found to contain 2000 ppb toluene and 1150 ppb naphthalene by gas chromatographic analysis. The procedure used in Example 7 was repeated and the results are shown in Table 6.

TABLE 6

<u>Total Volume (mL)</u>	<u>Toluene (ppb)</u>	<u>Naphthalene (ppb)</u>
Blank	2000	1150
100	<50	<20
300	<50	<20
500	<50	<20
700	<50	<20
900	<50	<20
1000	<50	<20

EXAMPLE 9

A pilot sized unit which consisted of a column 8 inches in diameter and 6 feet in height and which

possessed a 3 foot bed into which 1 cubic foot of XAD-16 resin was placed, was used to treat produced water from a production facility in California. The column was pre-treated prior to use by first passing fresh water followed by methanol over the column, each at a rate of 3.5 gallons per minute, for 15 minutes each. The samples taken for determination of soluble organics were analyzed by hand using Standard Method
 5 5520 C. The effluent stream was continuously monitored using the fluorescence method of the present invention over the same time period as was used for the soluble organic determinations. The fluorescence monitoring further was accomplished by comparison to the untreated water produced from the facility as a comparative blank sample.

The results of this comparative test are summarized in Figure 2 where it can be seen that the
 10 uppermost curve (filled circles) corresponds to time points obtained using continuous monitoring with the fluorescence detector and where the lowermost curve (open circles) corresponds to time points obtained during spot-checking using the standard analysis. As can be seen in this test, fluorescence detection compares favorably with standard analytical procedures.

15 Claims

1. A process for removal of water soluble organic compounds from produced water as defined herein, which is characterized by the steps of:
 - (a) directing a stream of produced water into a first column of adsorbing resin capable of
 20 accumulating water soluble organic compounds from the produced water and capable of producing an effluent with a reduced concentration of water soluble organic compounds;
 - (b) monitoring the concentration of water soluble organic compounds in the effluent of the first column of adsorbing resin;
 - (c) redirecting the stream of produced water into an alternate column of adsorbing resin capable of
 25 removing the water soluble organic compounds from the produced water and capable of producing an effluent having a reduced concentration of water soluble organic compounds;
 - (d) monitoring the concentration of water soluble organic compounds in the effluent of the alternate column of adsorbing resin;
 - (e) contacting the first column of adsorbing resin, which has accumulated water soluble organic
 30 compounds from the produced water, with a solvent capable of eluting accumulated amounts of the water soluble organic compounds from the adsorbing resin and capable of regenerating the adsorbing resin;
 - (f) redirecting the stream of produced water into the first column of adsorbing resin which has been regenerated as in step (e); and,
 - 35 (g) contacting the alternate column of adsorbing resin, which has accumulated water soluble organic compounds from the produced water, with a solvent capable of eluting the accumulated amounts of water soluble organic compounds from the adsorbing resin and capable of regenerating the adsorbing resin.
- 40 2. The process of claim 1 characterized in that the steps are carried out in a continuous fashion.
3. The process of claims 1 or 2 characterized in that a multiplicity of columns greater than two are used.
4. The process of claims 1, 2 or 3, characterized in that the adsorbing resin further comprises a
 45 nonionogenic, macroreticular adsorption resin, preferably a resin of polystyrene cross-linked with divinylbenzene.
5. The process of any of claims 1 to 4, characterized in that the water soluble organic compounds further comprise petroleum carboxylate salts, fatty acids, phenols, thiophenols, and petroleum-derived aromatic
 50 compounds.
6. The process of any of claims 1 to 5, characterized in that the monitoring of the concentration of water soluble organic compounds preferably involves monitoring the soluble organic concentration and further comprises conductivity measurement, fluorescence measurement, ultraviolet/visible adsorption mea-
 55 surement, turbidity measurement and infrared adsorption measurement.
7. The process of claim 6 characterized in that the fluorescence measurement further comprises continuously monitoring the effluent by continuously passing a portion of the effluent stream through a

fluorescence detector and wherein the fluorescence measurement is preferably carried out on naphthenic carboxylates.

8. The process of any of the preceding claims, characterized in that a regeneration of the columns of adsorbing resin with solvent preferably comprising acetone, isopropanol, ethanol, or methanol, together with a wash agent capable of removing dispersed oil from the resin, is followed by treatment of the resin with steam to remove residual solvent, and wherein condensate is preferably recovered from the steam treatment of the resin and added back to the eluting solvent.
9. The process of any of the preceding claims characterized in that an additional monitoring step is carried out on the eluting solvent to determine the concentration of water soluble organic compounds therein.
10. The process of claim 9 characterized in that the eluting solvent is purified by removing the water soluble organic compounds, preferably being continuous and also the purification of the eluting solvent comprising distillation, ion exchange, solvent stripping, evaporation and membrane filtration.
11. The process of claim 10 characterized in that the distillation of the eluting solvent includes the steps of directing the eluting solvent through a distillation system which distillation system comprises an incoming produced water source for heating the eluting solvent under vacuum and an ambient temperature water source for condensing the eluting solvent vapors.
12. The process of claim 10 or 11, characterized in that the organic compounds removed from the eluting solvent are recovered and preferably returned to an oil stream.
13. A process for removal and recovery of water soluble organic compounds from water removed from an oil well as a byproduct of crude oil production, which is characterized by the steps of:
 - (a) directing a stream of produced water into a first column containing a nonionogenic macroreticular resin capable of accumulating petroleum derived water soluble organic compounds from the water and capable of producing an effluent with a reduced concentration of petroleum derived water soluble organic compounds;
 - (b) monitoring the concentration of petroleum derived water soluble organic compounds in the effluent of the first column of adsorbing resin by monitoring the soluble organic concentration;
 - (c) redirecting the stream of produced water into an alternate column containing a nonionogenic macroreticular resin capable of accumulating petroleum derived water soluble organic compounds from the water and capable of producing an effluent with a reduced concentration of petroleum derived water soluble organic compounds;
 - (d) monitoring the concentration of petroleum derived water soluble organic compounds in the effluent of the alternate column of adsorbing resin by monitoring the soluble organic concentration;
 - (e) regenerating the first column of resin which has accumulated petroleum derived water soluble organic compounds from the produced water by regenerating with an eluting solvent;
 - (f) redirecting the stream of produced water into the first column of resin which has been regenerated as in step (e);
 - (g) regenerating the alternate column of resin which has accumulated petroleum derived water soluble organic compounds from the produced water by regenerating with an eluting solvent;
 - (h) purifying the eluting solvent used to regenerate the resin in steps (e) and (g) by continuous distillation;
 - (i) recovering the petroleum derived water soluble organic compounds from the distillation of the eluting solvent and returning the petroleum derived soluble organic compounds to an oil stream.
 - (j) repeating steps (a) through (i) in a continuous fashion.
14. The process of claim 13, wherein the monitoring conducted in steps (b) and (d) of the concentration of petroleum derived water soluble organic compounds in the effluent of the first and alternate columns, respectively, of adsorbing resin is performed by continuously monitoring the soluble organic concentration with a fluorescence detector.
15. The process of claim 13 or 14, wherein the regeneration of the first and alternate columns of resin performed in steps (e) and (g), respectively, is completed by removing residual eluting solvent using

steam treatment of the resin, the condensate of which steam treatment is returned to the eluting solvent.

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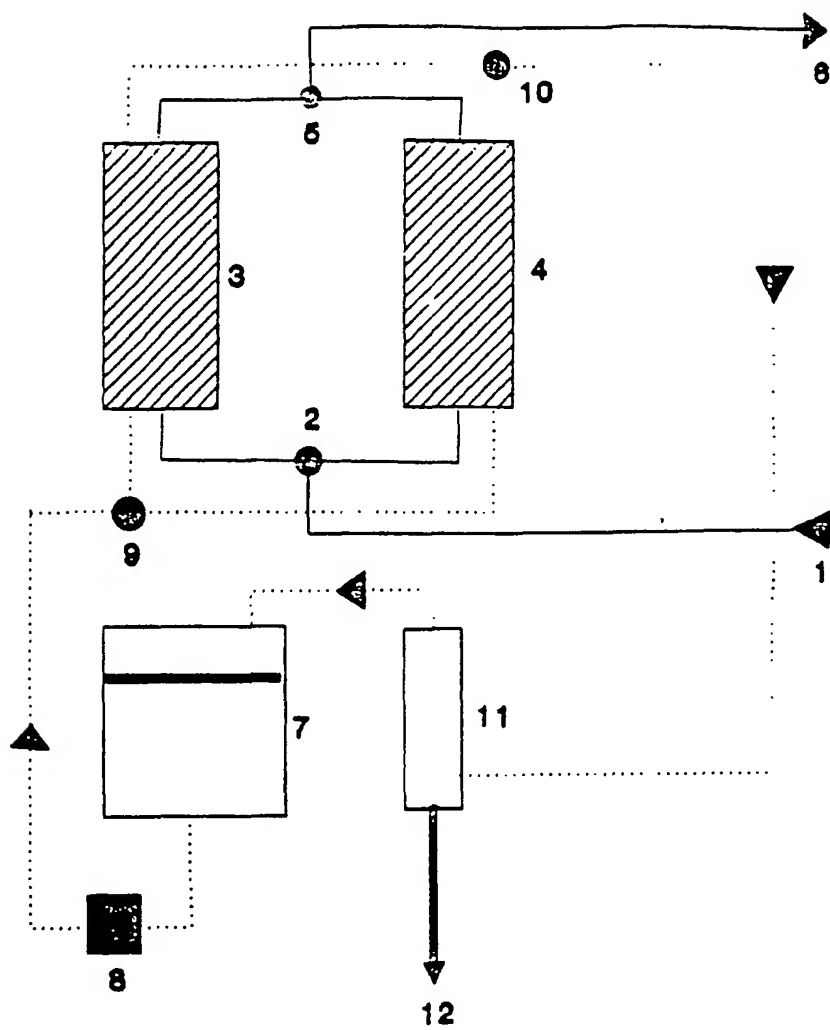
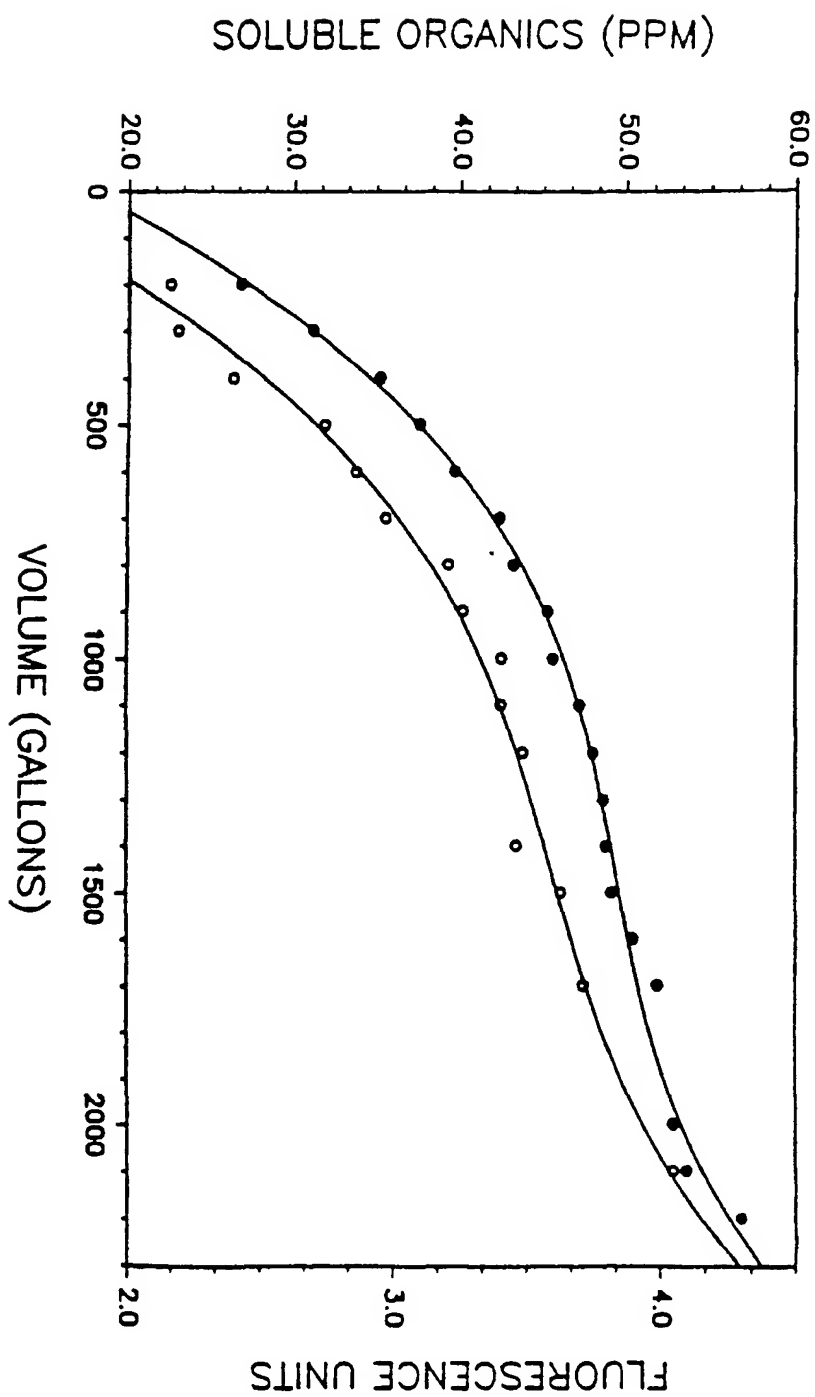


FIGURE 1

FIGURE 2

PILOT UNIT FIELD TEST, UNOCAL MANDALAY
RUN 2, 1-31-90





European Patent
Office

EUROPEAN SEARCH REPORT

Application Number

DOCUMENTS CONSIDERED TO BE RELEVANT			EP 90124160.4
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 5)
A	<u>DE - B2 - 2 818 729</u> (GEBRÜDER SULZER AG) * Column 4, line 54 - column 6; fig. 1,2 *	1-3, 13	C 02 F 1/28 C 02 F 1/40
A	<u>US - A - 3 855 123</u> (STRUDGEON et al.) * Column 4, line 66 - column 7, line 42; fig. 3,4 *	1, 2, 13	
A	<u>DD - A5 - 283 795</u> (BALTIISKOE MORSKOE PAROK-HODSTVO) * Pages 5,6; fig. *	1, 2	
D,A	<u>US - A - 4 775 475</u> (JOHNSON) * Column 7, line 12 - column 8, line 2; fig. *	1	
D,A	<u>US - A - 4 297 220</u> (MEITZNER et al.) * Claims 1,2 *	4	TECHNICAL FIELDS SEARCHED (Int. Cl. 5)
D,A	<u>CA - A - 1 103 170</u> (ROHM AND HAAS COMPANY) * Claims 1,4,5 *	4	C 02 F B 01 D 24/00
The present search report has been drawn up for all claims			
Place of search VIENNA		Date of completion of the search 07-03-1991	Examiner WILFLINGER
CATEGORY OF CITED DOCUMENTS X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document		I : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document	